

# ENZYME CATALYZED PROCESS FOR LOW COST CO<sub>2</sub> SEPARATION AND CAPTURE

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> Paper # 120 2012 MEGA Conference Baltimore, MD August 22, 2012

## **AGENDA**

- Introduction
- Akermin Technology
  - Enzymes
  - Benefits
  - Results of Economic Modeling
  - Laboratory Test Results
- DOE Pilot Project
- Conclusions



## AKERMIN, INC.

- St. Louis-based biotechnology company
- Developing next generation cost and energy efficient, environmentally benign systems for CO<sub>2</sub> capture
- 22 FTEs; seven Ph.Ds
- Funded by VCs and strategic investors
- Combining biochemistry, nanotechnology and engineering to develop and commercialize a novel, low-cost solution for carbon management









### THE CHALLENGE

### CO<sub>2</sub> Management Today

## Driving the Need is Growth in:

- Process industries requiring CO<sub>2</sub> capture
- Supply/demand for natural gas
- Demand for EOR
- CO<sub>2</sub> emissions
- Carbon capture regulations
- CO<sub>2</sub> feedstock for mineralization and bio-utilization

- Expensive, need dramatic cost reductions
- Political and regulatory uncertainties
- Revenue plays hampered by costs
- Dominant solution: Amine solvents
  - Reliable, yet expensive
  - Environmentally undesirable & require special handling
  - Issues with degradation and corrosion
  - High investment cost and energy consumption
- Delay in large-scale adoption

Growth, uncertainty and cost create CO<sub>2</sub> management opportunities



## **OUR FOCUS**

'Bridging the gap' to provide a biocatalyst-enabled industrial solution

### **Biocatalysts**

- Nature's perfect solution, Carbonic Anhydrase
- Over 100 times faster than best amines
- Short life in industrial process

### Akermin's Solution: Putting Enzymes to Work

- Solves problem of economic delivery of biocatalyst
- Protects biocatalyst using unique, proprietary polymer films
- Combines biochemistry and nanotechnology with engineering
- Capital-light using partnership model
- Scalable
- Compatible for new and existing systems
- Simple and environmentally-friendly approach

#### **Customer Needs**

- Continuous processes
- Robust solutions
- Reduced capital intensity
- Simplified process
- Flexible/adaptable
- Low lifecycle cost

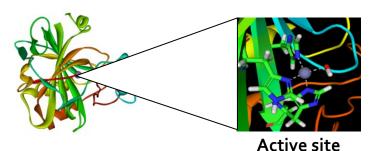
Disruptive Solution for CO<sub>2</sub> Management

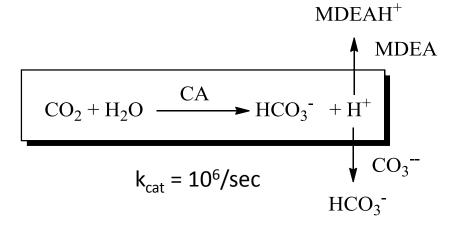


### **OUR SOLUTION**

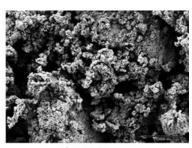
### Biocatalyst Delivery System

### Carbonic Anhydrase (CA)





CA is integrated in polymer with high surface area to minimize diffusional limitations



5kV 2500x mag



- Uses nature's best tool, CA, to accelerate CO<sub>2</sub> absorption
- Integrates biocatalyst into scalable low-cost proprietary polymer film
  - Maximizes performance
  - Extends biocatalyst lifetime
- Works with conventional mass-transfer devices
  - Reduces scale-up risk



### **KEY BENEFITS**

### Total cost of capture over 30% less than optimized amine systems

### Reduced capital costs

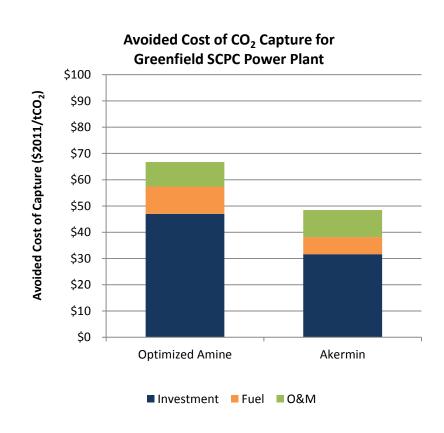
- No polishing FGD
- No wash columns
- Minimal/no intercooling
- No reforming
- Reduced requirements for solution handling & storage

### Reduced operating costs

- Lower costs for solution replacement
- Lower cooling requirements; water consumption
- Energy-efficient process; development target of 2.5 GJ/t-CO<sub>3</sub>

### Environmentally-friendly

- No solvent emissions to the atmosphere
- Produces benign by-products with low disposal costs, opportunities for resale

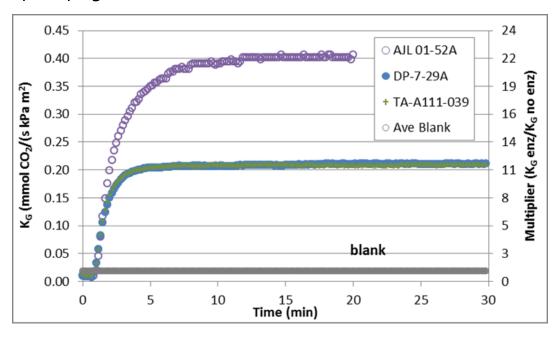


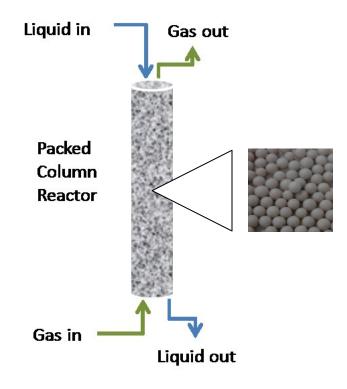
Enables a simple process chemistry and design that yields a low-cost solution for CO<sub>2</sub> capture



## PERFORMANCE OF BIOCATALYST IN A COUNTER-CURRENT FLOW COLUMN

20% Lean  $CO_2$  loading at room temperature p = 1 psig





Note: K<sub>c</sub> reported per packing area, lab-scale test reactor interfacial area ~ 30%

Up to 22-fold increase of K<sub>G</sub> was demonstrated

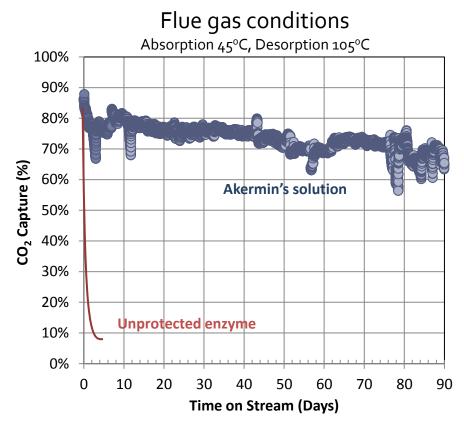


## LONG-TERM PERFORMANCE

Confirmed commercially-viable performance levels



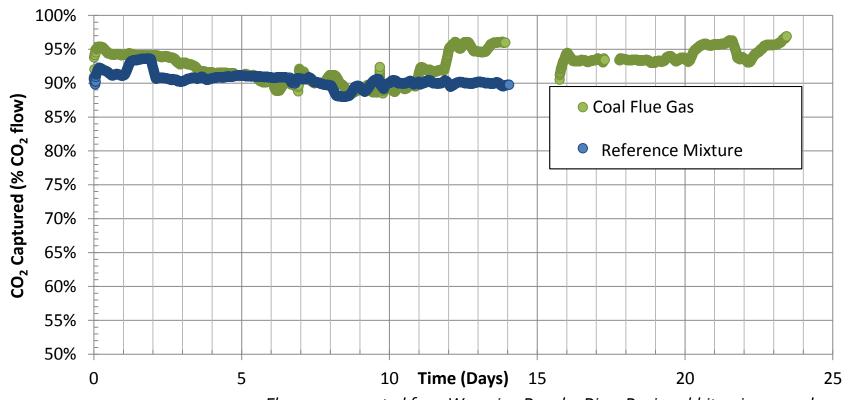
**Akermin's Closed Loop Reactor** 



Over 20 million CO<sub>2</sub> molecules hydrated by one CA molecule over 90 days Translates into > 400 kg CO<sub>3</sub> captured per day per kg of CA



## **TESTING ON FLUE GAS**



Flue gas generated from Wyoming Powder River Basin subbituminous coal Total mercury content ( $Hg^{2+}$  and  $Hg^{o}$ ) ~ 2ppbw

 $\sim$  90-95% CO<sub>2</sub> capture sustained for over 23 days on flue gas ( $\sim$ 14% feed) Overall performance is stable and comparable with reference



## DOE PILOT PROJECT

Demonstrate Biocatalyst delivery system on power plant flue gas

## Project participants







- Project duration: 33 months (initiated in October 2010)
- Funding

Total Project: \$ 4,750,000

DOE Funding: \$ 2,910,000

Akermin Cost share: \$ 1,840,000

200x scale-up from bench-scale, closed loop reactor



## TESTING AT THE NATIONAL CARBON CAPTURE CENTER (NCCC)



Flue gas drawn from downstream of FGD and returned upstream so any contaminants introduced are removed by FGD before passing to stack.

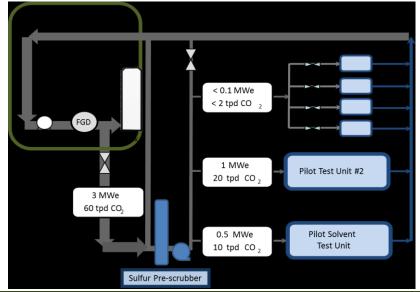
Akermin scheduled to commission pilot plant in 4<sup>th</sup> quarter of 2012; testing for up to six months.

Post-Combustion CO<sub>2</sub> Capture Center (PC<sub>4</sub>) part of the National Carbon Capture Center (NCCC).

Located adjacent to Alabama Power's Plant Gaston.

Established in 2009 through transition of Power Systems Development Facility and supported through funding from the US DOE.

PC4 commissioned in March 2011.





## KEY PROJECT OBJECTIVES - PHASE II

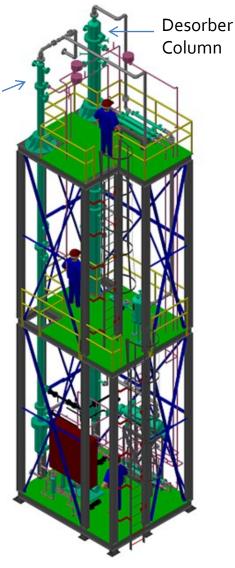
- Engineer Bench-Scale Carbon Capture System
  - 500 SLPM (5 to 10 kWe)
- Capture CO<sub>2</sub> from flue gas slip-stream for up to six months:
  - Demonstrate 90% CO<sub>2</sub> capture in presence of biocatalyst and potassium carbonate
  - Demonstrate long-term activity of biocatalyst delivery system
  - Characterize rate enhancement of biocatalyst delivery system
  - Demonstrate tolerance to flue gas impurities
  - Evaluate impact of external conditions on process performance
- Generate data to refine simulation models and confirm key advantages
- Model capital and operating costs for commercial-scale system



## **BENCH UNIT SPECIFICATIONS**

Absorber \_\_\_\_\_

- Overall dimensions (LxWxH): 10' X 12' X 49'
- Absorber Design Case
  - 500 SLPM flue gas (nominal)
  - Sulzer 500 m²/m³ packing
  - Nominal Liquid: 300 kg/hr
  - 20 wt% K<sub>2</sub>CO<sub>3</sub>
- Heat recuperative cross exchanger and trim coolers
- Emerson Delta-V Control System





## **UPCOMING ACTIVITIES**

Fabrication of Bench Unit	June – October 2012
Scale-up coating process and coat contactor	November 2012
Install/Commission	November 2012
Initial Testing (blank)	December 2012
Initial Testing (biocatalyst)	January 2013
Operate unit for six months	January – June 2013
Model and evaluate the capital operational costs for full-scale coal-fired power plant	June 2013





### **PROJECT TEAM**

### **AKERMIN:**

Dr. Alex Zaks, PM; VP, Research & CTO

John Reardon, PI; Director, Engineering

Dr. Tizah Anjeh, Senior Scientist

Dr. Tracy Bucholz, Senior Scientist

Dr. Matt Hulvey, Senior Scientist

Dr. Brett Rambo, Senior Scientist

Dr. Mark Walker, Senior Scientist

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Alex Shaffer, Engineering Associate

Jonathan Tuttle, Engineering Associate

Luke Weber, Research Associate

### **PNNL:**

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Mark Bearden, Pl

Dr. James Collett, PI

Dale King, PI

### **BATTELLE:**

Bradley Chadwell, PM

**U.S. DOE-NETL** 

Andrew Jones, PM

Special thanks to Novozymes (enzyme supply) and Emerson (design and supply of bench unit controls and instrumentation)



### ACKNOWLEDGEMENT AND DISCLAIMER

**Acknowledgement**: This material is based upon work supported by the Department of Energy National Energy Technology Laboratory under Award Number DE-FE0004228.

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## **ANY QUESTIONS?**



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